

# Topological aspects of three-dimensional wakes behind rotary oscillating cylinders

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(Received 7 February 2002 and in revised form 12 February 2004)

The development of a three-dimensional viscous incompressible flow generated behind an infinitely long circular cylinder, impulsively started into rectilinear motion and rotationally oscillating, is studied computationally. The numerical scheme, an hybrid vortex method, is used to integrate the velocity–vorticity formulation of the Navier–Stokes equations. The Reynolds number considered is  $Re = 400$ , which is moderate though beyond the critical values  $Re_2 \simeq 190$  and  $Re'_2 \simeq 260$  for which the flow becomes spontaneously three-dimensional. The numerical method is explained and its main points are developed. This scheme is then applied to solve some two-dimensional problems, both in order to validate the method and to compute a nominal two-dimensional flow, required to measure the impact of three-dimensionality. The three-dimensional flow past a steady cylinder is also compared to benchmark simulations. Once the flow has become fully three-dimensional, beyond the transient regime and saturation of instabilities, the cylinder begins a rotary oscillation around its axis. Two kinds of rotations are considered: constant amplitude and several frequencies, and constant frequency and various amplitudes. When amplitude and frequency are high enough, the whole flow comes back to its two-dimensional state. This result gives a justification for two-dimensional computations in the literature related to rotating cylinders. For the first super-harmonic frequency of the flow, a parametric study is performed in order to find the impact of the amplitude on the topology of the flow. A bifurcation is clearly identified. Finally, the mechanisms involved in the return to a two-dimensional state are explained: the interaction between transverse instabilities and von Kármán streets is quantified by means of a correlation analysis.

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## 1. Introduction and related work

The description of the wake behind bluff bodies in a viscous flow is of fundamental importance in many engineering and scientific fields. The canonical case of the circular cylinder has been reported in numerous works, concerning experimentations as well as numerical investigations, in the simplified case of a plane or in the physical three-dimensional space. The interest in body rotation is mainly motivated by the possibility of modifying the wake generated downstream and the forces created by the wake on the body. Such studies throw light on mechanisms that reduce drag forces, which is a key point in aeronautics and other fields of application, described for example in Sümer & Fredsøe (1997).

Most prior works concerned either steady cylinders in three dimensions, or rotating cylinders in two dimensions, mainly due to restrictive Courant–Friedrich–Levy conditions and computational cost. Early three-dimensional measurements, for

a steady cylinder, are reported in Wieselsberger (1922), though the three-dimensional cylinder has been a field of active research during the 1990s.

For incompressible wakes generated by a circular cylinder, two of the governing non-dimensional parameters are the Reynolds number  $Re = U_\infty D/\nu$ , where  $D$  is the diameter of the cylinder,  $U_\infty$  the free-stream velocity and  $\nu$  the kinematic viscosity, and the Strouhal number  $S_t = fD/U_\infty$ , where  $f = 1/T$ ,  $T$  being the natural period of the flow.

It is now well known that the wake of a circular cylinder becomes spontaneously three-dimensional when  $Re \geq Re_2 = 190$ . The instabilities and non-spanwise structures of the flow have been exhibited experimentally by Williamson (1988), and later numerically by Tomboulides, Triantafyllou & Karniadakis (1992). Several contributors, such as Karniadakis & Triantafyllou (1992), Beaudan & Moin (1994), Thompson, Hourigan & Sheridan (1994, 1996), Persillon & Braza (1998) and Kravchenko, Moin & Shariff (1999), have since studied the transition to turbulence and other aspects of these flows. Several diagnostics of the three-dimensional flows have been computed, by Henderson (1995a) and Mittal (1996), in order to provide an analysis of three-dimensional effects and comparison with experimental results such as in Williamson (1996). Higher Reynolds numbers have been also considered in the later works, for example Mittal (1996) or Jordan (1997), who have considered subgrid models.

It has been shown in Barkley & Henderson (1996) that two modes of transition, commonly called Mode A and Mode B, occur respectively at  $Re_2 \simeq 189$  and  $Re'_2 \simeq 259$ . Consequently, realistic numerical simulations have to be performed in three-dimensions when  $Re \geq 190$ .

When the cylinder is moving in steady or oscillating rotation, or oscillating in translation (i.e. vibration), the condition of linear stability implies that time steps have to be very small (hence the usual restriction to two-dimensional computations). The first two-dimensional numerical simulations of a more complex motion than a uniform translation dealt with the steadily rotating cylinder, initially by Coutanceau & M enard (1985) and Badr & Dennis (1985), followed by Chang & Chern (1991) and Chen, Ou & Pearlstein (1993) among others. Badr *et al.* (1990) combines experiments and numerical investigations in the range  $10^3 \leq Re \leq 10^4$ . Oscillating flows, i.e. pure oscillating translation, unlike uniform or accelerated motions, have been and are still a major field of interest in naval research. Properties of these flows have been studied for wide ranges of Keulegan–Carpenter numbers by many researchers, for example Bearman (1997). On the other hand, studies on cylinders oscillating freely under crosswise translation and undergoing uniform rectilinear motion have been performed over the last few years, both numerically by Blackburn & Henderson (1999) and experimentally by Govardhan & Williamson (2000). The same kind of problem with forced oscillations is developed in D utch *et al.* (1998), who combined numerical simulation and experimentation.

The motion considered in the present paper is a uniform rectilinear motion with rotational oscillation. This type of motion has been experimentally studied for low Reynolds numbers by Tameda (1978), who has provided snapshots of streamlines, and by Tokumaru & Dimotakis (1991) at  $Re = 15\,000$ . Numerical simulations corresponding to this case have been performed by Lu & Sato (1996), Chou (1997) and Baek & Sung (1998). Accurate numerical simulations can be found in the recent papers by Dennis, Nguyen & Kocabiyik (2000) and He *et al.* (2000), which are considered in the present paper as benchmarks for diagnostics. When rotations of higher amplitude are considered, diagnostics can be compared to the two-dimensional study by Milano *et al.* (2000) and Milano & Koumoutsakos (2002).

So far all the numerical simulations for rotating cylinders seem to have focused on two-dimensional geometries, probably due to the computational cost of three-dimensional simulations and available numerical tools. In order to be realistic, for long time scales and for Reynolds numbers above 190, numerical simulations should take into account the three-dimensionality of the flow. To perform such numerical simulations, a robust numerical method has to be used, i.e. which still converges when used with large time steps, in order to reach large time scales.

The goal of the present paper is to describe three-dimensional aspects of flows around a rotating cylinder that is infinitely long. This cylinder is steady until the flow is fully three-dimensional, at  $Re = 400$ . Then the cylinder begins to rotate, with an angular position given by the formula

$$\theta(t) = -A \cos(\pi S_F t)$$

with  $S_F$  being the *forced Strouhal number* and  $A$  the peak angular position, called *amplitude*. Consequently, the tangential velocity on the body is given by  $V = R\dot{\theta} = A\pi S_F R \sin(\pi S_F t)$ . The ratio  $S_F/S_t$  will be chosen as integer in order to consider only harmonic and super-harmonic frequencies of the flow. This avoids focusing on locking phenomena and competition between different frequencies.

The main result presented herein is that the flow comes back to a two-dimensional state in the neighbourhood of the body for high amplitudes. The question of the critical amplitude that leads to a two-dimensional flow is also considered in the case for which  $S_F/S_t = 2$ .

Furthermore, fast rotations can lead to a substantial drop in the drag coefficient. This fact has been exhibited experimentally in Tokumaru & Dimotakis (1991) (at  $Re = 1.5 \times 10^4$ ) and numerically in Milano *et al.* (2000). For medium-range frequencies of rotation, refer to Dennis *et al.* (2000) and He *et al.* (2000).

An outline of the present paper is as follows. The numerical method is first described in §2, and a few two-dimensional diagnostics are computed in §3, in order to provide a validation of the numerical scheme. The present results are compared to two-dimensional computations by Henderson (1995*b*, 1997), Utne (1997), Blackburn & Henderson (1999), Dennis *et al.* (2000) and He *et al.* (2000). Section 4 shows the spontaneous development of three-dimensionality. For  $Re = 400 \geq Re'_2 = 260$ , mode B is identified by means of spectrum analysis, and diagnostics are compared to Barkley & Henderson (1996), Henderson (1995*a*) and Wieselsberger (1922). The development of three-dimensionality is shown to be exponential. Section 5 shows the effect of a high amplitude of rotation ( $A = \pi/2$ ) for a few frequencies, and exhibits representative phenomena due to the body rotation. The effect of the amplitude on the topology of the flow is then discussed in §6 for  $S_F/S_t = 2$ . Finally, in §7, the mechanism leading to a two-dimensional flow is identified and discussed in the case  $S_F/S_t = 2$  and  $A = \pi/2$ , and a correlation analysis is provided.

## 2. The three-dimensional Navier–Stokes equations

The present numerical method is a deterministic hybrid Vortex-In-Cell method (particles carry vorticity, see Cottet & Koumoutsakos (2000) for general overview). Fields which are solutions of Poisson or Helmholtz equations are computed on a cylindrical grid instead of considering a pure Lagrangian method. Recent developments in these methods for both two- and three-dimensional flow computations are described in Cottet & Poncet (2002, 2003), based on preliminary results presented

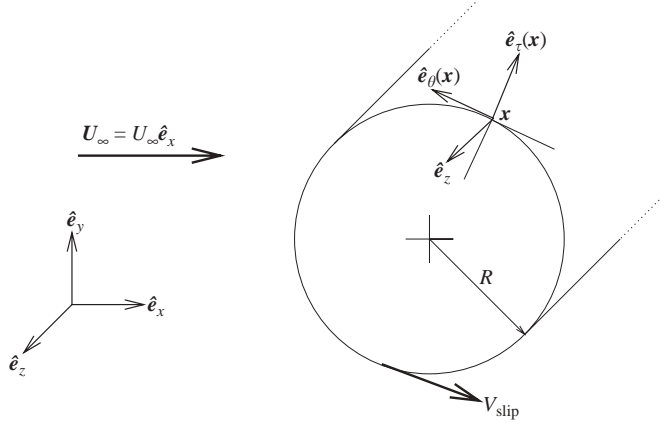


FIGURE 1. Cartesian and cylindrical coordinate basis.

in Cottet *et al.* (2002), Koumoutsakos & Leonard (1995) and Ould-Sahili, Cottet & El Hamraoui (2000) for wake computations.

Let us consider the three-dimensional Navier–Stokes equations in their fully nonlinear velocity–vorticity formulation

$$\frac{\partial \boldsymbol{\omega}}{\partial t} + \mathbf{u} \cdot \nabla \boldsymbol{\omega} - \boldsymbol{\omega} \cdot \nabla \mathbf{u} - \nu \nabla^2 \boldsymbol{\omega} = 0 \quad (2.1a)$$

where  $\nabla$  is a gradient operator,  $\nu$  is the kinematic viscosity,  $\boldsymbol{\omega}$  is the vorticity field and  $\mathbf{u}$  is the velocity field, satisfying

$$\nabla \cdot \mathbf{u} = 0, \quad \nabla \times \mathbf{u} = \boldsymbol{\omega}. \quad (2.1b)$$

Thus  $\nabla \cdot \boldsymbol{\omega} = 0$ . We also consider a smooth three-dimensional body  $\mathcal{B}$ , which is an infinitely long circular cylinder. On this cylinder there is the no-slip boundary condition

$$\mathbf{u} = V_{\text{slip}} \hat{\mathbf{e}}_{\theta} \quad (2.1c)$$

where  $V_{\text{slip}}$  is the tangential body velocity. If the cylinder is not rotating, then  $V_{\text{slip}} = 0$ .

Throughout this paper, the far-field condition is

$$\mathbf{u}(x) \rightarrow \mathbf{U}_{\infty} \quad \text{as } |x| \rightarrow \infty, \quad (2.1d)$$

and since the cylinder is infinitely long, all functions are periodic in the spanwise direction. This period is denoted by  $L$ . In order to simplify notation, these two last boundary conditions will no longer be written.

The basis is written  $(\hat{\mathbf{e}}_x, \hat{\mathbf{e}}_y, \hat{\mathbf{e}}_z)$  in Cartesian coordinates and  $(\hat{\mathbf{e}}_r, \hat{\mathbf{e}}_{\theta}, \hat{\mathbf{e}}_z)$  in cylindrical coordinates (see figure 1). The vector  $\hat{\mathbf{e}}_x$  is in the streamwise direction and  $\hat{\mathbf{e}}_y$  in the crosswise direction. Throughout this paper, the body  $\mathcal{B}$  is a circular cylinder, whose axis is in the spanwise direction  $\hat{\mathbf{e}}_z$ . The computational domain is then  $\Omega = \mathbb{R}^3 \setminus \overline{\mathcal{B}}$ .

### 2.1. Particle methods

In order to solve numerically the Navier–Stokes equations, we consider a Lagrangian ‘Particle-in-Cell’ method. This method, described below, is based on a hybrid formulation of vortex methods.

Particles carry cells of vorticity, and velocity reconstruction uses Helmholtz and Poisson equations via back and forth interpolations on a grid, instead of a classical

approach using multipole methods or stochastic methods such as Monte-Carlo. This leads to a gain of accuracy (compared to Monte-Carlo methods) and speed (compared to the multipole approach, see Cottet & Poncet 2002).

Let the particles be indexed by  $p = 1 \dots n$ . A particle is described by its position  $\mathbf{x}_p(t)$ , its vorticity  $\boldsymbol{\omega}_p(t)$ , and its volume  $v_p$ . This volume does not depend on time due to the incompressibility. Thus one considers solutions in the form

$$\boldsymbol{\omega}(t) = \sum_{p=1}^n \boldsymbol{\omega}_p(t) \delta_{\mathbf{x}_p(t)} v_p \quad (2.2)$$

where  $\delta_{\mathbf{x}_p}$  is the Dirac function at  $\mathbf{x}_p$ .

The no-slip condition (2.1c) may be written in a scalar form, with a no-slip condition

$$\mathbf{u} \cdot \widehat{\mathbf{e}}_r = 0 \quad (2.3a)$$

and the two tangential conditions

$$\mathbf{u} \cdot \widehat{\mathbf{e}}_\theta = V_{\text{slip}}, \quad \mathbf{u} \cdot \widehat{\mathbf{e}}_z = 0. \quad (2.3b)$$

A fractional-step algorithm is then used to solve the Navier–Stokes equations (2.1a–c) with the measure solution (2.2). Let  $\boldsymbol{\omega}_0$  be a measure solution at time  $t_0$ .

The first step is pure convection, which ensures the no-slip condition (2.3a):

$$\left. \begin{aligned} \frac{d\boldsymbol{\omega}_p}{dt} &= [\nabla \cdot (\mathbf{u} \otimes \boldsymbol{\omega})]_{\mathbf{x}_p(t)}, \\ \frac{d\mathbf{x}_p}{dt} &= \mathbf{u}(\mathbf{x}_p(t)), \end{aligned} \right\} \quad (2.4)$$

for  $t \in [t_0, t_0 + \delta t]$ , where fields  $\mathbf{u}$  and  $\boldsymbol{\omega}$  satisfy

$$\left. \begin{aligned} \nabla \times \mathbf{u} &= \boldsymbol{\omega}, & \nabla \cdot \mathbf{u} &= 0 & \text{in } \Omega \times [t_0, t_0 + \delta t], \\ \boldsymbol{\omega}(t_0) &= \boldsymbol{\omega}_0 & & & \text{on } \Omega, \\ \mathbf{u} \cdot \widehat{\mathbf{e}}_r &= 0 & & & \text{on } \partial\Omega \times [t_0, t_0 + \delta t]. \end{aligned} \right\} \quad (2.5)$$

The stretching tensor  $\nabla \cdot (\mathbf{u} \otimes \boldsymbol{\omega})$  is equal to  $\boldsymbol{\omega} \cdot \nabla \mathbf{u}$  when  $\nabla \cdot \boldsymbol{\omega} = 0$ . This tensor makes the numerical scheme more stable when the vorticity is not algebraically divergence-free. It remains to treat the diffusion and the tangential no-slip condition (2.3b). The main difficulty of step (2.4) is the computation of the velocity field, which is discussed in the following subsection.

## 2.2. Velocity computation and grid–particle coupling

The initial data of step (2.4) are the vorticity field  $\boldsymbol{\omega}_0$ . This field contains the position, the pointwise vorticity and the volume of all particles. Thus step (2.4) is a classical dynamical system once the velocity field is known. This velocity must satisfy

$$\left. \begin{aligned} \nabla \times \mathbf{u} &= \boldsymbol{\omega} & \text{on } \Omega, \\ \nabla \cdot \mathbf{u} &= 0 & \text{on } \Omega, \\ \mathbf{u} \cdot \widehat{\mathbf{e}}_r &= 0 & \text{on } \partial\Omega. \end{aligned} \right\} \quad (2.6)$$

The usual deterministic approach of vortex methods is to compute this velocity field with the Biot–Savart laws:

$$\mathbf{u}(x_q) = [K_\varepsilon * \boldsymbol{\omega}](x_q) = \int_{\Omega} K_\varepsilon(x_q - x) \boldsymbol{\omega}(x) dx = \sum_{x_p} K_\varepsilon(x_q - x_p) \boldsymbol{\omega}(x_p) v_p$$

given the particle description (2.2) of the vorticity. Such an approach requires  $n^2$  evaluations of the mollified Green kernel  $K_\varepsilon$ ,  $n$  being the number of particles. This computation is not yet technically possible for three-dimensional computations involving millions of particles (see Cottet & Poncet 2002, 2003) in time-dependent simulations, despite recent advances in multipole methods by Strickland *et al.* (1999), Plouhmans & Winckelmans (2000) and Lindsay & Krasny (2001).

An alternative way to compute the velocity field is to use a stream function  $\psi$ . For any divergence-free vorticity field and at any time  $t$ , the link between the stream function and vorticity is

$$-\nabla^2 \psi = \omega \quad (2.7a)$$

with arbitrary boundary conditions which imply  $\nabla \cdot \psi = 0$  (thus  $\psi$  is globally divergence-free). We also consider a harmonic potential  $\phi$ , i.e.

$$\nabla^2 \phi = 0 \quad (2.7b)$$

which satisfies

$$\frac{\partial \phi}{\partial n} = \nabla \times \psi \cdot \widehat{e}_r$$

on the boundary  $\partial\Omega$ . Eventually the velocity is computed by the Helmholtz decomposition

$$\mathbf{u} = \nabla \times \psi - \nabla \phi$$

and satisfies equations (2.6).

In order to solve the Poisson equations (2.7a,b), the vorticity is interpolated onto a grid. The velocity is computed on this grid and interpolated back to particles. Such a method is called *hybrid* due to the fact that it uses both particles and grids. The interpolation is a third-order tensor product formula (see Monaghan 1985), except near the body where one-sided formulae are preferred. Details of this strategy of interpolation can be found in Cottet & Poncet (2003).

### 2.3. Diffusion and boundary layer

Our approach is an extension to three-dimensions of the method used by Koumoutsakos, Leonard & Pepin (1994) to study two-dimensional diffusion and vorticity boundary conditions. Diffusion in the fluid, the second step of the fractional-step algorithm, is performed through vorticity exchange among particles. The no-slip condition (third step) is enforced by means of a vorticity flux at the boundary.

More precisely, let  $\omega_1$  be the final value at  $t = t_0 + \delta t$  of the first step (2.4). The vorticity field on the boundary can be written in cylindrical coordinates  $\omega = (\omega_r, \omega_\theta, \omega_z)$ . The diffusion is given by the heat equation:

$$\left. \begin{aligned} \frac{\partial \omega}{\partial t} &= \nu \nabla^2 \omega && \text{in } \Omega \times [t_0, t_0 + \delta t], \\ \frac{\partial \omega_z}{\partial n} &= 0 && \text{on } \partial\Omega \times [t_0, t_0 + \delta t], \\ \kappa \omega_\theta + \frac{\partial \omega_\theta}{\partial n} &= 0 && \text{on } \partial\Omega \times [t_0, t_0 + \delta t], \\ \omega_r &= 0 && \text{on } \partial\Omega \times [t_0, t_0 + \delta t], \\ \omega(t_0) &= \omega_1 && \text{on } \Omega, \end{aligned} \right\} \quad (2.8)$$

where  $\kappa = 1/R$  is the curvature of the cylinder. For a small viscosity  $\nu$ , i.e. for a high enough Reynolds number, this equation can be solved with an explicit scheme, a ‘Particle Strength Exchange’ algorithm, developed in Degond & Mas-Gallic (1989).

Let  $\omega_2$  be the solution of (2.8). Furthermore, for any  $t$  between  $t_0$  and  $t_0 + \delta t$ , the velocity produced by the solution of (2.8) is written  $\mathbf{u}_{spu}(t)$  and is commonly called spurious velocity. This velocity  $\mathbf{u}_{spu}(t)$  is computed by solving equation (2.6).

The no-slip condition (2.3b) is enforced by means of the boundary layer. This viscous boundary layer is step 3 of the fractional-step algorithm, another heat equation:

$$\left. \begin{aligned} \frac{\partial \boldsymbol{\omega}}{\partial t} &= \nu \nabla^2 \boldsymbol{\omega} && \text{on } \Omega \times [t_0, t_0 + \delta t], \\ \nu \frac{\partial \omega_z}{\partial n} &= -\frac{\partial \mathbf{u}_{spu}}{\partial t} \cdot \widehat{\mathbf{e}}_\theta - \frac{\partial V_{\text{slip}}}{\partial t} && \text{on } \partial \Omega \times [t_0, t_0 + \delta t], \\ \nu \kappa \omega_\theta + \frac{\partial \omega_\theta}{\partial n} &= \frac{\partial \mathbf{u}_{spu}}{\partial t} \cdot \widehat{\mathbf{e}}_z && \text{on } \partial \Omega \times [t_0, t_0 + \delta t], \\ \omega_r &= 0 && \text{on } \partial \Omega \times [t_0, t_0 + \delta t], \\ \boldsymbol{\omega}(t_0) &= 0 && \text{on } \Omega, \end{aligned} \right\} \quad (2.9)$$

where  $V_{\text{slip}} = R\dot{\theta}$  is the velocity on the surface of the body due to the rotation. The Robin boundary conditions enforce  $\partial_t \nabla \cdot \boldsymbol{\omega} = 0$ . We have

$$\begin{aligned} \frac{\partial}{\partial r}(\nabla \cdot \boldsymbol{\omega}) &= \left( \nabla^2 \omega_r - \frac{\omega_r}{r^2} - \frac{2}{r^2} \frac{\partial \omega_\theta}{\partial \theta} \right) + \frac{1}{r^2} \frac{\partial \omega_\theta}{\partial \theta} + \frac{1}{r} \frac{\partial}{\partial \theta} \frac{\partial \omega_\theta}{\partial r} + \frac{\partial}{\partial z} \frac{\partial \omega_z}{\partial r} \\ &= (\nabla^2 \boldsymbol{\omega}) \cdot \mathbf{e}_r + \frac{1}{r} \frac{\partial}{\partial \theta} \left( \frac{1}{r} \omega_\theta \right) + \frac{1}{r} \frac{\partial}{\partial \theta} \frac{\partial \omega_\theta}{\partial r} + \frac{\partial}{\partial z} \frac{\partial \omega_z}{\partial r} \\ &= \frac{1}{\nu} \frac{\partial \omega_r}{\partial t} + \frac{1}{r} \frac{\partial}{\partial \theta} \left( \kappa \omega_\theta + \frac{\partial \omega_\theta}{\partial r} \right) + \frac{\partial}{\partial z} \frac{\partial \omega_z}{\partial r} \\ &= \frac{1}{\nu} \frac{\partial}{\partial t} \frac{\partial \mathbf{u}_{spu} \cdot \mathbf{e}_z}{r \partial \theta} - \frac{1}{\nu} \frac{\partial}{\partial t} \frac{\partial \mathbf{u}_{spu} \cdot \widehat{\mathbf{e}}_\theta}{\partial z} \\ &= \frac{1}{\nu} \frac{\partial}{\partial t} (\nabla \times \mathbf{u}_{spu} \cdot \mathbf{e}_r) = \frac{1}{\nu} \frac{\partial}{\partial t} (\boldsymbol{\omega}_2 \cdot \widehat{\mathbf{e}}_r) = 0. \end{aligned}$$

Consequently, divergence satisfies the well-posed heat equation

$$\left. \begin{aligned} \frac{\partial (\nabla \cdot \boldsymbol{\omega})}{\partial t} - \nu \nabla^2 (\nabla \cdot \boldsymbol{\omega}) &= 0 && \text{in } \Omega \times ]t_0, t_0 + \delta t[, \\ \nabla \cdot \boldsymbol{\omega}(t_0) &= 0 && \text{on } \Omega, \\ \frac{\partial}{\partial r} (\nabla \cdot \boldsymbol{\omega}) &= 0 && \text{on } \partial \Omega \times ]t_0, t_0 + \delta t[, \end{aligned} \right\}$$

and thus remains zero over time and space.

The solution of (2.9) can be computed in its integral form, see Friedmann (1964) and Koumoutsakos *et al.* (1994):

$$\boldsymbol{\omega}(x, t) = \int_{t_0}^t \int_{\partial \Omega} G(x, t; \xi, \tau) \boldsymbol{\mu}(\xi, \tau) d\xi d\tau$$

where  $G$  is the three-dimensional heat kernel, with  $\tau < t$ :

$$G(x, t; \xi, \tau) = (4\pi\nu(t - \tau))^{-3/2} \exp\left(-\frac{\|x - \xi\|^2}{4\nu(t - \tau)}\right)$$

and  $\boldsymbol{\mu}$  a weighted field defined on the physical boundary. The construction of this weighted field is based on the first-order development of the integral equation satisfied by  $\boldsymbol{\mu}$ , and does not create divergence, as seen above (see Cottet & Poncet 2003). This technique is a very robust and flexible algorithm for boundary layer computation, and

can be used in various situations involving tangential velocities (see control strategies in Poncet & Cottet 2003; Cottet & Poncet 2004; and Poncet & Koumoutsakos 2004).

#### 2.4. Conclusions the numerical scheme

A fractional step algorithm (2.4), (2.8), (2.9) has been developed in order to approximate the solutions of the Navier–Stokes equations. The first step, given by equation (2.4), is a convection step. The second one is the diffusion step, given by the heat equation (2.8). The third and last step is the boundary layer computation, defined by equation (2.9). It enforces the no-slip conditions (2.3b). Moreover, particles are periodically remeshed, mainly using the third-order kernel introduced by Monaghan (1985).

If we write as respectively  $\omega_2$  and  $\omega_3$  the solutions of (2.8) and (2.9) at  $t = t_0 + \delta t$ , then  $\omega_2 + \omega_3$  is a second-order approximation of the solution of the Navier–Stokes equations (2.1a–c) at  $t = t_0 + \delta t$ .

The computational domain  $\Omega$  used for three-dimensional simulations at  $Re = 400$  is an ‘O-grid’ defined by

$$R \leq r \leq R + 4\pi R \quad \text{and} \quad -2\pi R \leq z \leq 2\pi R.$$

The discretization is  $256 \times 128 \times 128$  for the variables  $r$ ,  $\theta$  and  $z$  respectively. The great stability of the Lagrangian method allows one to use a non-dimensional time step  $U_\infty \delta t / R = 0.1$ . The solver takes about 145 s per time step with the resolution above, which means about 35  $\mu$ s per grid point on a DEC- $\alpha$  server.

#### 2.5. Mechanical diagnostics

The non-dimensional time  $t$  depends on the dimensional time  $t^*$  through the relation

$$t = \frac{U_\infty t^*}{R}.$$

From now on only the non-dimensional time  $t$  will be used.

The Reynolds number is defined as

$$Re = \frac{U_\infty D}{\nu}$$

and the non-dimensional frequency of the flow, i.e. the Strouhal number, is defined as

$$St = \frac{f D}{U_\infty} \quad (2.10)$$

where  $f = 1/T$  is the natural frequency of the flow. The drag and lift coefficients are computed as in Koumoutsakos & Leonard (1995). The friction coefficients are defined by

$$C_{DF} = -\frac{\nu}{U_\infty^2 RL} \int_{\partial\Omega} \omega_z \sin \theta \, ds, \quad C_{LF} = \frac{\nu}{U_\infty^2 RL} \int_{\partial\Omega} \omega_z \cos \theta \, ds,$$

and the pressure coefficients by

$$C_{DP} = -\frac{\nu}{U_\infty^2 RL} \int_{\partial\Omega} \frac{\partial \omega_z}{\partial r} r \sin \theta \, ds, \quad C_{LP} = \frac{\nu}{U_\infty^2 RL} \int_{\partial\Omega} \frac{\partial \omega_z}{\partial r} r \cos \theta \, ds.$$

Thus the expression for the drag coefficient is

$$C_D = C_{DF} + C_{DP} \quad (2.11a)$$



(a)	$Re$	$\overline{C_D}$	$\widehat{C_L}$	$S_r$	(b)	$Re$	$\overline{C_D}$	$\widehat{C_L}$	$S_r$
	200	1.3389	$\pm 0.0015$	0.70	0.199	200	1.3412	0.700 <sup>†</sup>	0.1972, 0.196 <sup>†</sup>
	300	1.3820	$\pm 0.0031$	0.96	0.211	300	1.3769	–	0.2113
	400	1.4080	$\pm 0.0043$	1.08	0.2228	400	1.4142	–	0.2198
	500	1.4433	$\pm 0.0050$	1.23	0.230	500	1.4449	1.19 <sup>*</sup>	0.2254
	1000	1.5264	$\pm 0.0097$	1.45	0.241	1000	1.5191 <sup>‡</sup>	–	0.2372, 0.2392 <sup>‡</sup>

TABLE 1. Diagnostics for Reynolds numbers between 200 and 1000. (a) Present computations. (b) Henderson (1995b) and Henderson (1997), except \* Blackburn & Henderson (1999), † Utnes (1997) and ‡ He *et al.* (2000). The error on  $\overline{C_D}$  is the 90% confidence interval of the mean drag coefficient.

and the lift coefficient is

$$C_L = C_{LF} + C_{LP}. \quad (2.11b)$$

### 3. Drag coefficients of two-dimensional flows

In order to provide a validation of the numerical scheme and study the behaviour of the nominal two-dimensional flow, we perform several two-dimensional simulations. Since these two-dimensional computations exhibit the nominal state of forthcoming three-dimensional simulations, the Reynolds number is chosen in the range between 200 and 1000.

#### 3.1. Drag coefficient of a flow past a steady cylinder at various Reynolds numbers

In this section, a few values of the drag and lift coefficients are computed in the case of a two-dimensional flow.

The cylinder is impulsively started at  $t=0^+$ , and is slightly rotating during the early time with a tangential velocity  $V_{\text{slip}} = \sin(\pi t/2)$  when  $t \leq 4$ . This slight rotation is performed in order to break the crosswise symmetry of the flow. This triggers the first von Kármán instability, which would appear later otherwise, thus there is a gain of computational time since this aspect of the flow is not the topic of the present study. For  $t \geq 4$ , the cylinder is steady, i.e.  $V_{\text{slip}} = 0$ .

Figure 2 shows the drag and lift coefficient for various Reynolds numbers between 200 and 1000. Table 1 shows values of the mean value of the drag coefficient  $C_D$ , denoted  $\overline{C_D}$ , the mean of peak values of the absolute lift coefficient  $|C_L|$ , denoted  $\widehat{C_L}$ , and the Strouhal number  $S_r$ . In this table, one can compare the values found by the present method to the results of Henderson (1995b) and Blackburn & Henderson (1999). Note that Blackburn & Henderson (1999) gives a range of 1.18–1.20 for  $\widehat{C_L}$ , which emphasizes the sensitivity of this quantity. One can see a quite good agreement between the present values and the related works, especially for the drag coefficient plotted on figure 3. In order to get such an accuracy, the computational domain has been radially extended up to  $(1 + 8\pi)R$  for these two-dimensional simulations.

#### 3.2. Drag coefficient of a flow past a rotationally oscillating cylinder

This discussion on two-dimensional flows can be found in several forms in the existing literature. Note that Dennis *et al.* (2000) provides a lot of diagnostics for a rotary oscillating cylinder, especially for drag and lift coefficients.

The simulation begins as described in the last section, i.e. the symmetry of the flow is broken by a slight rotation before  $t \leq 4$ , and then the cylinder stays steady. At

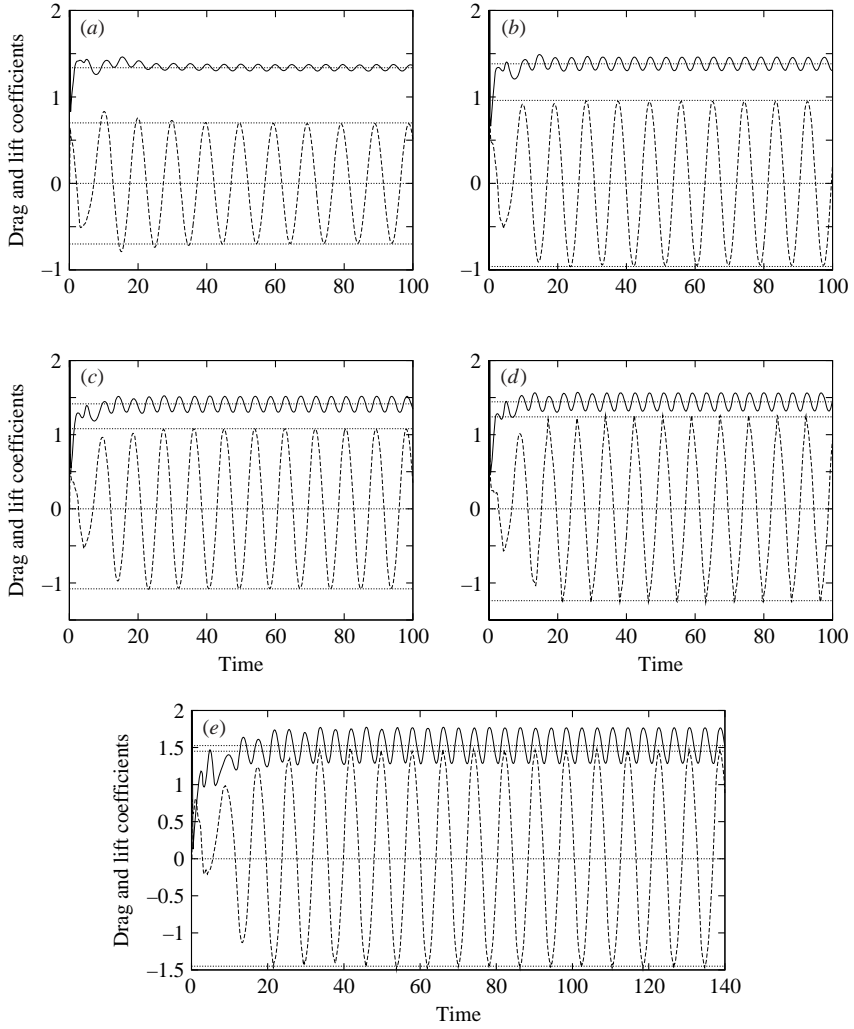


FIGURE 2. Drag and lift coefficients at  $Re = (a) 200, (b) 300, (c) 400, (d) 500$  and  $(e) 1000$ .  
 —,  $C_D$ ; - -,  $C_L$ ;  $\cdots$ , values from table 1.

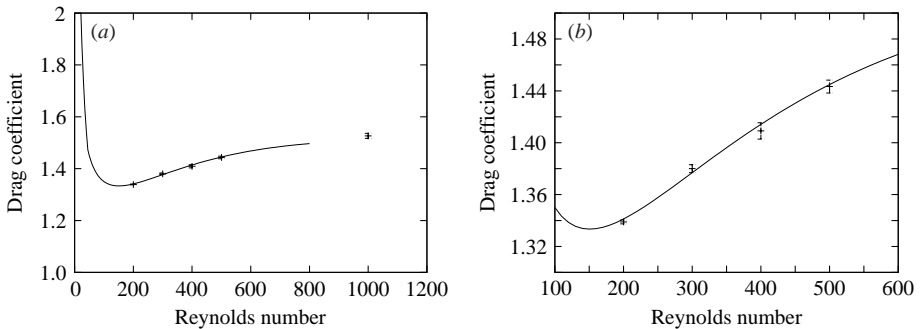
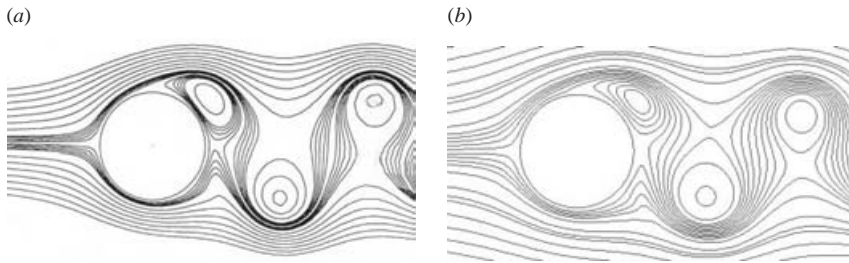


FIGURE 3. Comparison of two-dimensional drag coefficients between Henderson's benchmark values (—) and table 1 with 90% confidence intervals; (b) is a zoom of (a).

$S_F/S_t$	0	1.0	1.2	1.45	1.45	2.0	3.0
$A$	–	$\pi/2$	$\pi/2$	$\pi/2$	$3/\pi$	$\pi/2$	$\pi/2$
$V_{\max}$	0	1.135	1.362	1.646	1	2.270	3.405
$\overline{C_D}$	1.443	2.60	1.66	1.36	1.30	1.09	0.82

 TABLE 2. Mean drag coefficients at  $Re = 500$  for various rotation parameters ( $V_{\max} = A\pi S_F$ ).

 FIGURE 4. Streamlines at  $Re = 500$  for  $A = 3/\pi$  and  $S_F = 1/3 \simeq 1.45S_t$ , obtained by (a) Dennis *et al.* (2000), and (b) the present work. Part (a) was kindly provided by S.C.R. Dennis.

$t = 60$ , the rotation is activated. Our formula of the tangential velocity on the body is

$$V_{\text{slip}} = A\pi S_F R \sin(\pi S_F t) \quad (3.1)$$

where  $S_F$  is the forced Strouhal number,  $A$  the rotation amplitude and  $R$  the radius of the cylinder. The quantity  $S_F$  is defined in the same spirit as the natural Strouhal number  $S_t$  (see equation (2.10)), that is to say

$$S_F = \frac{f_c D}{U_\infty}$$

where  $f_c$  is the frequency of the cylinder rotation.

If a point on the cylinder is initially set at  $\theta(0) = -A$ , its location at time  $t$  is given by

$$\theta(t) = \theta(0) + \frac{1}{R} \int_0^t V_{\text{slip}}(u) du = -A \cos(\pi S_F t)$$

since  $V_{\text{slip}} = R\dot{\theta}$ . This makes the formula (3.1) especially interesting.

The forced Strouhal number  $S_F$  is chosen as a multiple of the natural Strouhal number  $S_t$ . Moreover, we will call *high amplitude* a rotation whose amplitude  $A$  is  $\pi/2$ .

It is known that a rotation whose amplitude and frequency are high enough (at least  $S_F = 2S_t$ ) leads to a substantial drop in the drag coefficient (cf. numerical investigations of He *et al.* 2000; Milano *et al.* 2000; Dennis *et al.* 2000). The drag coefficient may even decrease by a factor 2 for high Reynolds number, as shown in the experimental work by Tokumaru & Dimotakis (1991) at  $Re = 15000$ .

Table 2 shows the mean drag coefficients at  $Re = 500$  for a few forced Strouhal numbers from  $S_F = S_t$  up to  $S_F = 3S_t$ , with  $A = \pi/2$ . When  $S_F \leq 1.45S_t$ , the mean drag decreases. Moreover, the drag coefficient decreases by 25% for  $S_F = 2S_t$  and by 43% for  $S_F = 3S_t$ . A special case with  $S_F = 1/3$  and  $A = 3/\pi$  has been performed in order to compare with Dennis *et al.* (2000) (figure 4), whose cylinder is initially rotating. The present computation gives  $\overline{C_D} = 1.30$  which somewhat disagrees with

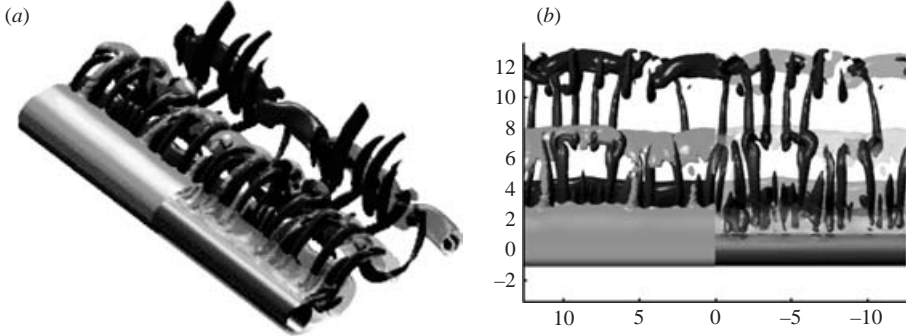


FIGURE 5. Three-dimensional structures of vorticity, present work at  $Re = 300$ , doubled spanwise by periodicity ( $t = 350$ ), with a clearer view of axial vorticity in (b).

Dennis *et al.* (2000) who find a value close to 1.11, but shows a good agreement on streamlines (see figure 4). Given the wide range of values for  $\overline{C_D}$  presented herein and in Dennis *et al.* (2000), He *et al.* (2000) and Milano *et al.* (2000), and given its sensitivity in Tokumaru & Dimotakis (1991), the accuracy of the present values of  $\overline{C_D}$  is questionable when the cylinder is rotating at high frequency. Nevertheless, the present computations and those provided by He *et al.* (2000) are compatible and seem to be converged.

#### 4. Three-dimensional flow past a steady cylinder

It is well known that the wake of a circular cylinder becomes spontaneously three-dimensional when  $Re > 190$ . This fact is thoroughly investigated and analysed in Barkley & Henderson (1996) for the linearized Navier–Stokes equations, and in the survey paper by Williamson (1996), for the experimental aspects. After this transition, the von Kármán streets are no longer spanwise invariant. If  $Re > 260$ , thinner structures appear as links between the streets, sometimes referred as ‘fingers’ of vorticity (cf. Jordan 1997). These thin structures correspond to the mode of instability called mode B, and Barkley & Henderson (1996) show that their wavelength is  $0.82D$ , and that they appear at  $Re = 259 \pm 2$ .

Since the present computations are performed at  $Re = 400$ , mode B is the dominant mode of instability (see figure 5) and we will focus our attention on its wavelength. We consider the Fourier transform of the velocity

$$\widehat{\mathbf{u}}_\beta(x, y) = \int_0^L \mathbf{u}(x, y, z) e^{-2i\pi\beta z/L} dz$$

which corresponds to a non-dimensional wavelength  $\lambda_z/D = L/\beta D$ . The axial energy spectrum is defined by

$$\|\widehat{\mathbf{u}}_\beta\|_2^2 = \int_{\mathbb{R}^2} |\widehat{\mathbf{u}}_\beta(x, y)|^2 dx dy$$

with respect to the non-dimensional wavelength  $\lambda_z/D$ .

This spectrum is plotted on figure 6, which shows a strong resonance around  $\lambda_z/D \simeq \pi/8$ , i.e. around 0.79. Furthermore, near the transition at  $Re'_2 = 260$ , the wavelength of mode B has been predicted close to  $\lambda_z/D = 0.82$  by Barkley & Henderson (1996). This wavelength can change as  $Re$  increases since the domain of unstable wavelengths becomes larger. One can even find several wavelengths

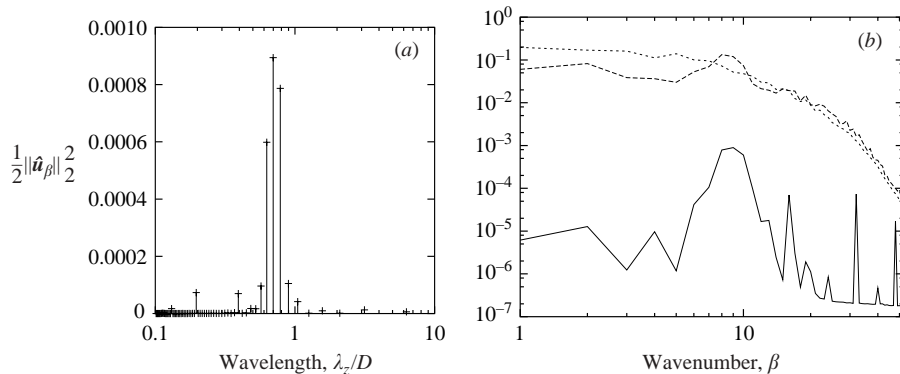


FIGURE 6. Axial energy spectrum at  $Re = 400$ . (a) Energy spectrum with respect to  $\lambda_z/D$  and its resonance at  $\lambda_z/D \simeq 0.73$ , at  $t = 60$  during the transient from two and to three-dimensions. (b) Energy spectra with respect to the modes  $\beta$  at  $t = 60$  (—),  $t = 100$  (---) and  $t = 150$  (- - -).

of mode B instability for a same Reynolds number, depending on the streamwise position, when  $Re > 600$  (see Barkley & Henderson 1996 and Persillon & Braza 1998). Mode B is the main mode of turbulence, at least until  $Re = 1900$  (see Unal & Rockwell 1988), where turbulence begins to govern the flow.

On the one hand, these properties justify the comparisons between flows at  $Re = 260$  and  $Re = 400$ . On the other hand, this explains why the velocity spectrum  $\beta \rightarrow \|\hat{\mathbf{u}}_\beta\|_2^2$  plotted on figure 6 is exponential and does not exhibit a  $-5/3$  power behaviour. In the range  $190 \leq Re \leq 2000$ , cylinder wakes are three-dimensional but not turbulent. Moreover, figure 6 shows the velocity spectra related to the development of the instabilities ( $t = 60$ ), the saturation of these instabilities ( $t = 100$ ), and when the three-dimensionality is fully developed (at  $t = 150$ ).

The evolution of the three-dimensionality inside the computational domain can be shown by means of the *transverse enstrophy*  $Z^\perp$  defined as follows:

$$Z^\perp = \frac{1}{2} (\|\omega_x\|_2^2 + \|\omega_y\|_2^2) = \frac{1}{2} \int_\Omega \omega_x^2(\xi) d\xi + \frac{1}{2} \int_\Omega \omega_y^2(\xi) d\xi$$

which is plotted with respect to time on figure 7. This gives the amount of transverse vorticity (vorticity which is not spanwise), and so is a measure of the three-dimensionality of the flow in the neighbourhood of the body. Figure 7 exhibits in more detail the phenomenon shown on the spectra of figure 6: at  $t \simeq 40$ , the non-axial noise becomes structured and the flow enters an exponential development of mode B, i.e.

$$\frac{1}{2} (\|\omega_x\|_2^2 + \|\omega_y\|_2^2) \simeq a e^{t/2.9}$$

with  $a = 7.14 \times 10^{-12}$ . At  $t \simeq 110$ , these instabilities saturate and the three-dimensionality is then fully developed. Note that this exponential behaviour is not noisy.

The spectral profile  $\mathfrak{P}$  is introduced in order to capture the spanwise structures for a given wavelength. This spectral profile is defined by

$$\mathfrak{P}_{\lambda_z/D}(x, y) = |\hat{\mathbf{u}}_{L/\lambda}(x, y)|^2. \quad (4.1)$$

Figure 8 shows this profile at the resonance wavelength, compared to the profile of

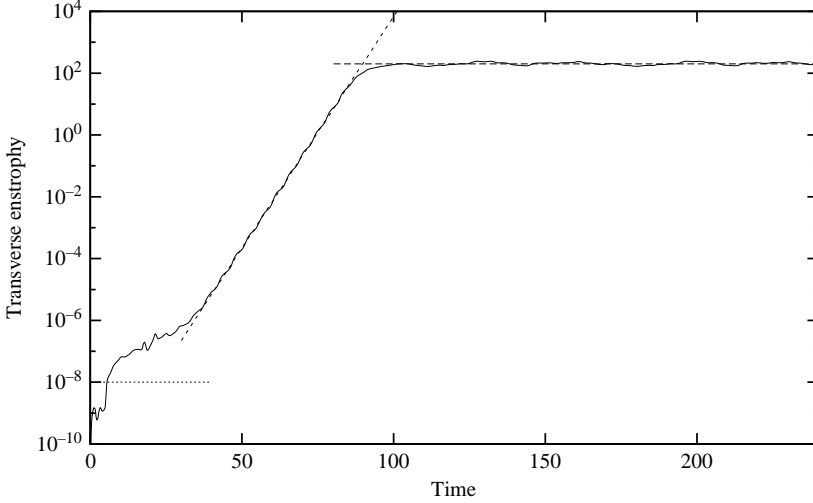


FIGURE 7. Development of transverse enstrophy  $Z^\perp = (\|\omega_x\|_2^2 + \|\omega_y\|_2^2)/2$  at  $Re = 400$ . Dashed lines show the constant value 200 and the exponential  $a e^{t/2.9}$  with  $a = 7.41 \times 10^{-12}$ .

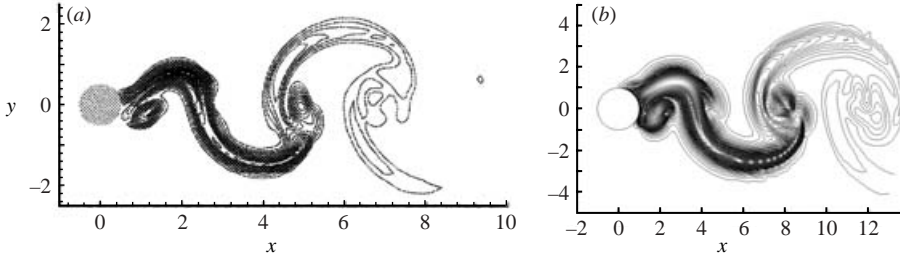


FIGURE 8. Isovalues of spectral profile at main growth mode. (a)  $\mathfrak{P}_{0.82}$  from Barkley & Henderson (1996) at  $Re = 260$ . (b)  $\mathfrak{P}_{0.79}$  from present work at  $Re = 400$ .

Barkley & Henderson (1996) at  $Re = 260$ . Once again the two results are in good agreement.

The effect of three-dimensionality on the drag coefficient  $C_D$  is plotted on figure 9, as well as the friction coefficient  $C_{DF}$ , the two-dimensional mean value at 1.41 from table 1, consistent with Henderson (1995b), and eventually the value 1.19, consistent with the three-dimensional experimental results by Wieselsberger (1922) and Jordan & Fromm (1972). The friction coefficient  $C_{DF}$  does not seem to be much affected by the strong three-dimensionality of the flow in the neighbourhood of the cylinder.

In addition to these diagnostics, one can also notice, on a more qualitative level, the great similarity between the present results and experimental snapshots provided by Williamson (1996). A surface of isovorticity obtained beyond the transient is plotted on figure 10 and compared to an experimental picture in Williamson (1996). The similarity concerns the spacing between von Kármán streets (due to the small dependency of the Strouhal number on the Reynolds number above  $Re'_2$ ), the topology of fingers of vorticity, the location and the size of knots, and local dislocations of spanwise streets.

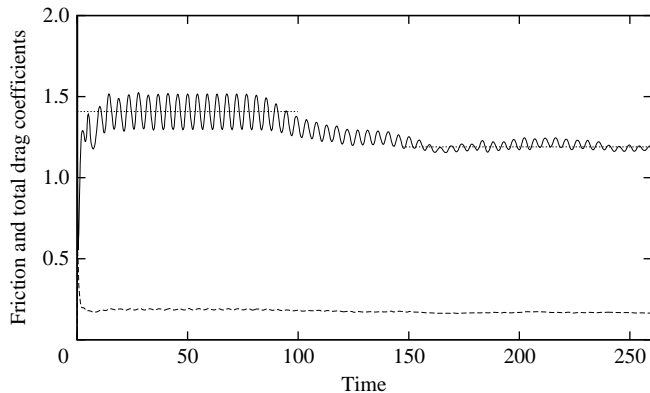


FIGURE 9. Effect of three-dimensionality on the drag coefficient  $C_D$  at  $Re = 400$ . The friction coefficient  $C_{DF}$  is plotted a dashed line. Dotted lines show values at 1.41 and 1.19.

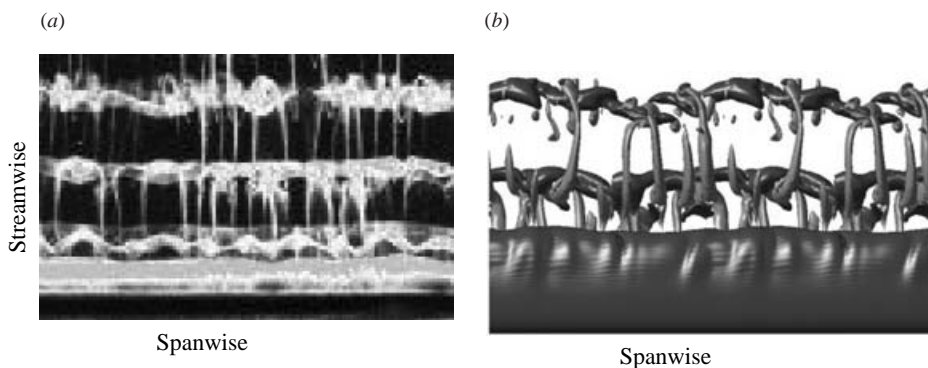


FIGURE 10. Visual comparison of three-dimensional structures of vorticity between experimentation (*a*, Williamson (1996) at  $Re = 270$ ) and present work (*b*, at  $Re = 400$ , doubled spanwise by periodicity,  $t = 160$ ).

### 5. Three-dimensional flows past a rotating cylinder with high-amplitude rotation

This section focuses on flows behind a cylinder rotating by half a revolution, i.e.  $A = \pi/2$ , with various rotation frequencies. The last section has shown that the three-dimensionality of the flow past a steady cylinder and its effects on diagnostics have been well resolved at  $Re = 400$ . Figure 7 shows that the saturated regime is reached around  $t \simeq 100$ . In order to avoid any transient effect, we wait for  $t = 160$  before activating the rotation. Then the cylinder begins to oscillate around its axis according to formula (3.1).

In order to find the effect of the rotation on the topology of the flow, several surfaces of isovorticity, at several levels and different times are plotted, for  $S_F = S_t$  and  $S_F = 2S_t$ . This is shown on figure 11, on which one can see the evolution of the three-dimensionality in the neighbourhood of the body by means of the *transverse vorticity*:

$$\omega^\perp = (\omega_x^2 + \omega_y^2)^{1/2}.$$

One can see on figure 11 that the three-dimensionality tends to disappear (see also Poncet 2002). Indeed, only a small quantity of transverse vorticity remains at  $t = 240$

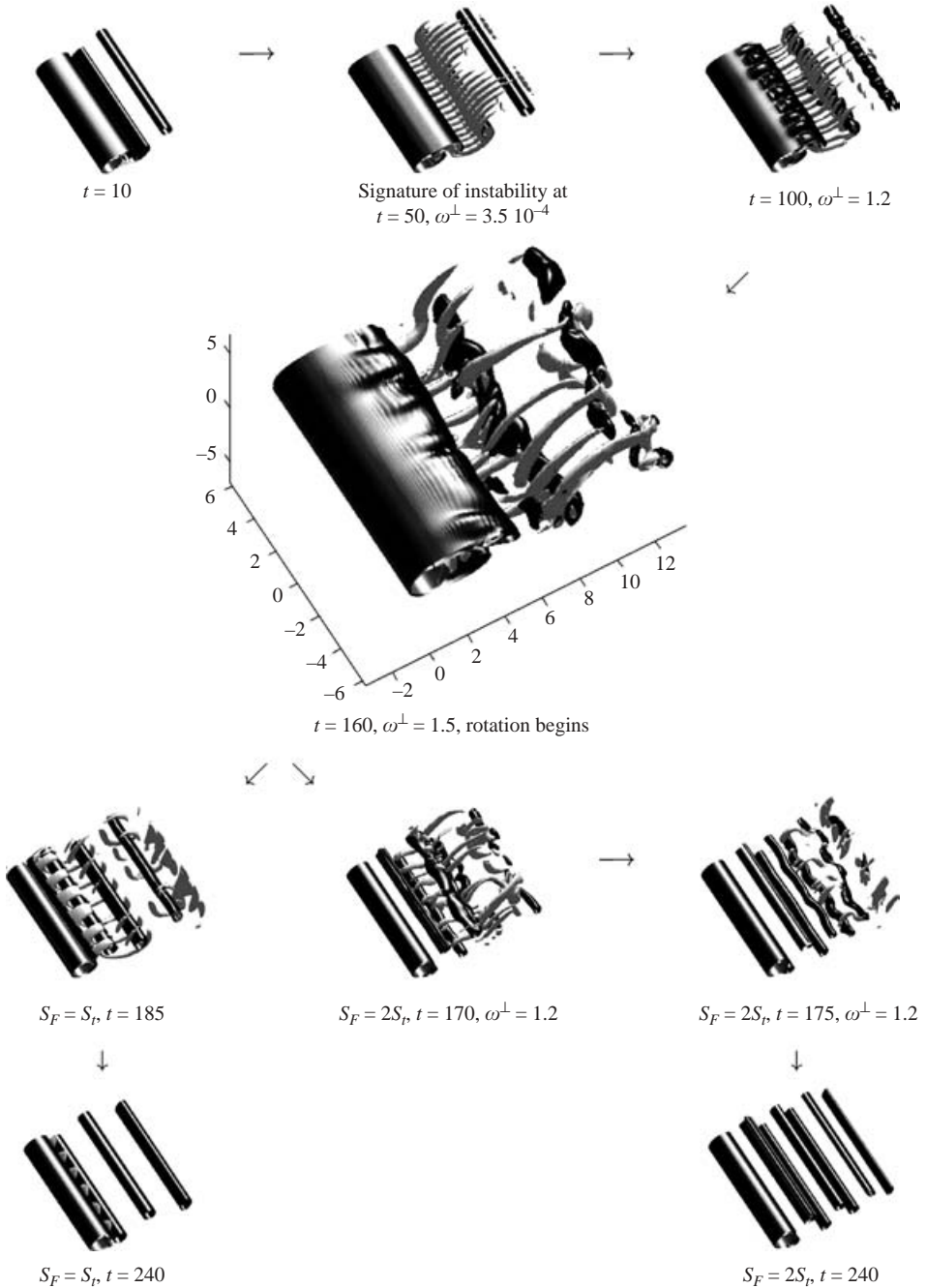


FIGURE 11. Effect of half a full rotation on the shape of the flow at  $Re = 400$ . Surfaces of spanwise isovorticity  $\omega_z = \pm 1.2$  and transverse vorticity  $\omega^\perp = 0.25$  unless written otherwise, for frequencies  $S_F = S_t$  and  $S_F = 2S_t$ .

when  $S_F = S_t$ , i.e. when the rotation frequency is locked at the natural frequency of the flow  $S_t = 0.223$ . Moreover, one can also see that no visible three-dimensionality remains at  $t = 240$  at the higher frequency  $S_F = 2S_t$ , i.e. when the rotation frequency is the first superharmonic of the nominal flow.



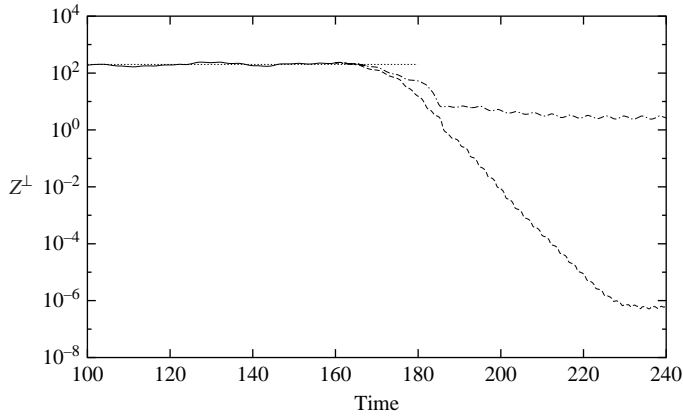


FIGURE 12. Transverse enstrophy  $Z^\perp$  at  $Re = 400$  with respect to time, for a rotation amplitude  $A = \pi/2$ . —,  $S_F = 2S_t$ ; ···,  $S_F = S_t$ .

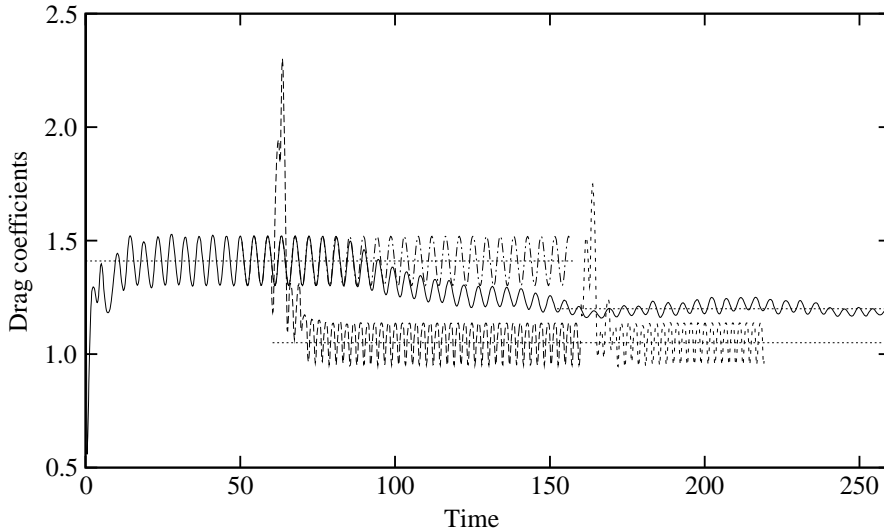


FIGURE 13. Effect of body rotation on the drag coefficient  $C_D$  at  $Re = 400$ , with  $S_F = 2S_t$  and  $A = \pi/2$ . —, Steady and three-dimensional; ···, steady and two-dimensional; - - -, rotation two-dimensional; - · - ·, rotation three-dimensional. Dotted lines show values at 1.05, 1.19 and 1.41.

This phenomenon is quantified on figure 12, which shows the transverse enstrophy  $Z^\perp$ , i.e. half the mean square of transverse vorticity over the computational domain. One can see that with superharmonic rotation with the transverse enstrophy decreases down to  $5 \times 10^{-7}$ , which corresponds to  $2 \times 10^{-13}$  per particle (and roughly half per grid point). Consequently we can say that the flow is totally two-dimensional in a large neighbourhood of the cylinder. Also, when  $S_F = S_t$ , the transverse enstrophy tends to a mean value of 3.05, which means that the global three-dimensionality is divided by 65, i.e. decreases by 98.5%.

Since the flow comes back to a two-dimensional state when  $S_F = 2S_t$ , the drag coefficient  $C_D$  should be compared to the drag coefficient of the two-dimensional rotating cylinder. This comparison is shown on figure 13, where we can see that

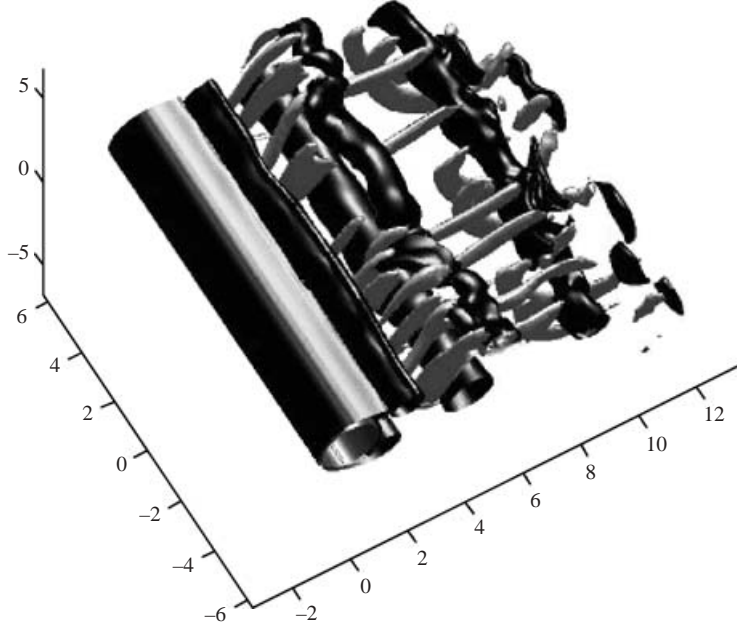


FIGURE 14. Isovorticity surface at  $t = 255$ ,  $Re = 400$ ,  $S_F = 2S_t$  and  $A = \pi/5$ .

both the two-dimensional and three-dimensional computations lead to a mean drag coefficient value of 1.05. The nominal two-dimensional drag coefficient is 1.41, and the three-dimensional unforced drag coefficient is 1.19: this means a drop of 12% from the three-dimensional flow and 26% from the two-dimensional flow.

## 6. Effect of the amplitude on three-dimensionality

In order to study the effect of the amplitude on the three-dimensionality of the flow, we have to consider a constant frequency. Indeed, for a given frequency, for example  $S_F = 2S_t$ , we have seen in the last section that with an amplitude of  $A = \pi/2$  the flow comes back to its two-dimensional state. This is not the same for  $A = \pi/5$ , in which case the flow remains three-dimensional, as it can be seen on figure 14.

The question addressed in this section is to find a critical value  $A_0$  which separates two- and three-dimensional flows. This critical amplitude depends on the rotation frequency  $S_F$  and on the Reynolds number: given the computational cost of these simulations, it is too ambitious to consider a parametric study of the bifurcation.

Consequently, we focus on the case  $Re = 400$  and  $S_F = 2S_t$ , and search for a small interval of values of  $A$  for which the top of the interval leads to a two-dimensional flow and the bottom of the interval leads to a three-dimensional flow. The tool which allows us to decide whether the flow is two-dimensional or three-dimensional in the neighbourhood  $\Omega$  of the body is the same as in last section, i.e. the transverse enstrophy:

$$Z^\perp = \frac{1}{2} (\|\omega_x\|_2^2 + \|\omega_y\|_2^2) = \frac{1}{2} \int_\Omega \omega_x^2(\xi) d\xi + \frac{1}{2} \int_\Omega \omega_y^2(\xi) d\xi.$$

As a first approach, one can plot  $Z^\perp$  for a wide range of amplitudes  $A$ . Figure 15 shows these curves for amplitudes from  $A = \pi/5$  up to  $A = \pi/2$  with a logarithmic scale. On this figure, three curves, corresponding to  $A = \pi/2$ ,  $A = 2\pi/5$  and  $A = \pi/3$ , lead

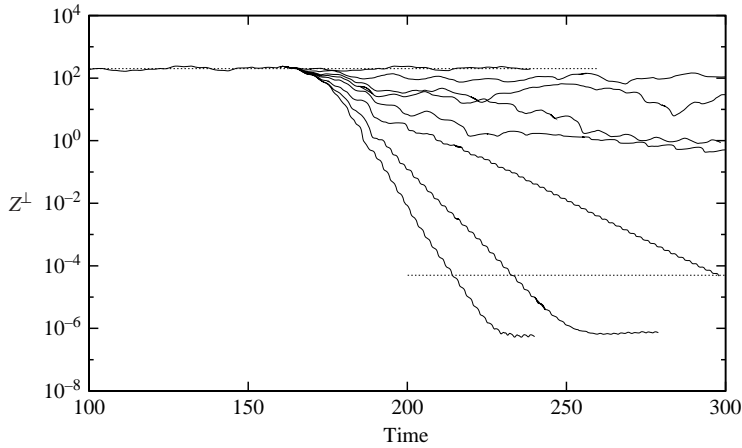


FIGURE 15. Transverse enstrophy  $Z^\perp$  at  $Re=400$  with respect to time, for several rotation amplitudes, in a logarithmic scale. From bottom to top:  $A = \pi/2$ ,  $A = 2\pi/5$ ,  $A = \pi/3$ ,  $A = 2\pi/7$ ,  $A = \pi/3.75$ ,  $A = \pi/4$ ,  $A = \pi/5$  and  $A = 0$  (steady).

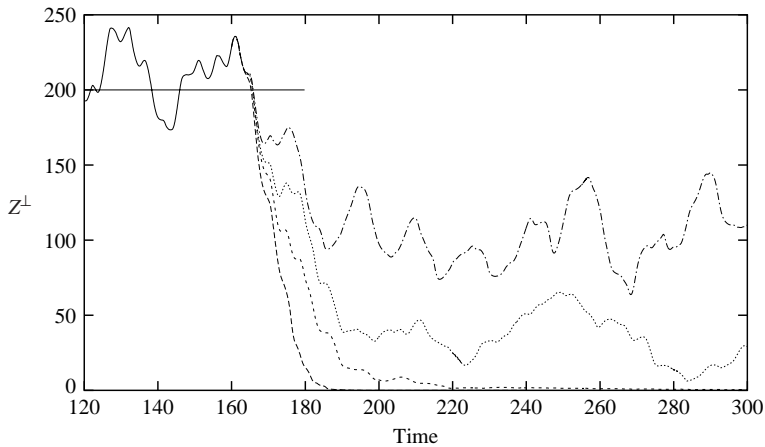


FIGURE 16. Transverse enstrophy  $Z^\perp$  at  $Re=400$  with respect to time, for several rotation amplitudes in a linear scale. From bottom to top:  $A = \pi/2$ ,  $A = \pi/3.5$ ,  $A = \pi/4$  and  $A = \pi/5$ .

clearly to a two-dimensional flow. The two curves above, i.e.  $A = \pi/3.5$  and  $A = \pi/3.75$ , do not seem to decrease down to zero. Nevertheless, between the activation of the rotation at  $t_c = 160$  and  $t = 300$ , the mean transverse enstrophy becomes more than 400 times smaller, thus one can consider that this flow is two-dimensional. In order to clarify this property, the same quantity is plotted without a logarithmic scale on figure 16. One can check that  $A = 2\pi/7 = \pi/3.5$  can indeed be considered as a two-dimensional flow. The two last curves of figure 15 show that amplitudes  $A \leq \pi/4$  allow the flow to stay three-dimensional in the neighbourhood of the body. Once again, as an example, figure 14 shows such a flow, for  $A = \pi/5$ .

The bifurcation can then be tracked between  $A = 2\pi/7$  and  $A = \pi/4$ . In order to locate the critical value, five amplitudes  $A = \pi/\alpha$  have been tested,  $\alpha$  being 3.5, 3.75, 3.8, 3.9 and 4. The result is plotted on figure 17, and by means of this figure, the critical value  $A_0$  is located in the interval  $\pi/3.8 \leq A_0 \leq \pi/3.9$ : figure 18 shows the transverse enstrophy for these two values. Note that this critical value depends

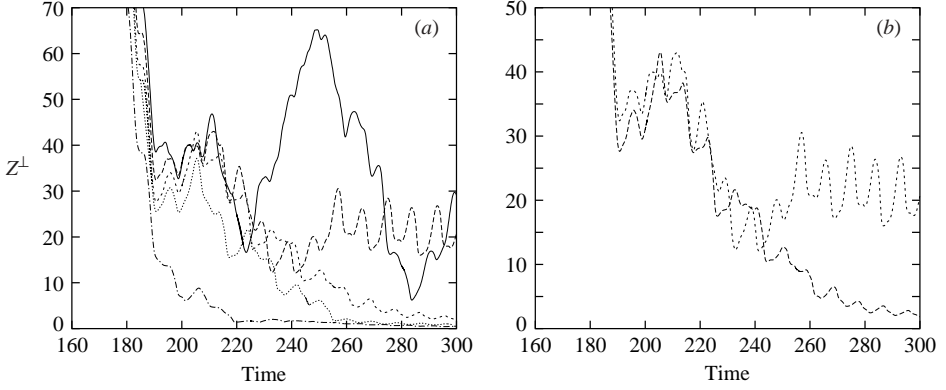


FIGURE 17. Transverse enstrophy  $Z^\perp$  at  $Re = 400$  with respect to time, for several rotation amplitudes close to the bifurcation value. (a) From bottom to top:  $A = 10\pi/35$ ,  $A = 10\pi/37.5$ ,  $A = 10\pi/38$ ,  $A = 10\pi/39$  and  $A = 10\pi/40$ ; (b) only amplitudes  $A = \pi/3.8$  and  $A = \pi/3.9$ .

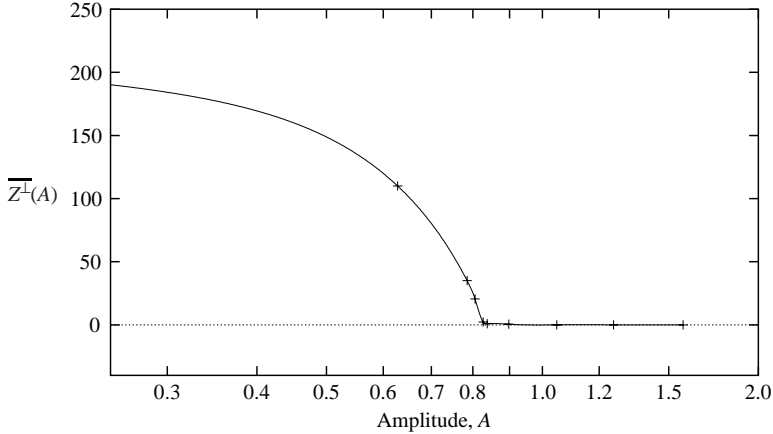


FIGURE 18. Mean residual transverse enstrophy  $\overline{Z^\perp}$  (defined in text) with respect to the rotation amplitude  $A$ , at  $Re = 400$ ,  $S_F = 2S_r$ . +, Computations; —, curve linking the points by interpolation.

slightly on the computational domain, because at this amplitude a larger domain would contain a small amount of three-dimensional structures of vorticity. Indeed, one must keep in mind that we focus on the amount of three-dimensionality in the (large) neighbourhood  $r \leq (1 + 4\pi)R$  of the body.

An open question is the dynamic of these three-dimensional structures. Indeed, they can either follow the potential stream and leave infinitely far away from the body, or, as suspected but not proved, reach a critical distance where three-dimensionality is stable. The computational cost required to prove this is currently far out of reach.

To summarize all these computations, one can plot the mean residual transverse enstrophy between  $t_1 = 250$  and  $t_2 = 300$ :

$$\begin{aligned} \overline{Z^\perp} &= \frac{1}{t_2 - t_1} \int_{t_1}^{t_2} Z^\perp(t) dt = \frac{1}{2(t_2 - t_1)} \int_{t_1}^{t_2} \|\omega_x(t)\|_2^2 + \|\omega_y(t)\|_2^2 dt \\ &= \frac{1}{2(t_2 - t_1)} \int_{t_1}^{t_2} \int_{\Omega} \omega_x(\xi, t)^2 + \omega_y(\xi, t)^2 d\xi dt \end{aligned}$$

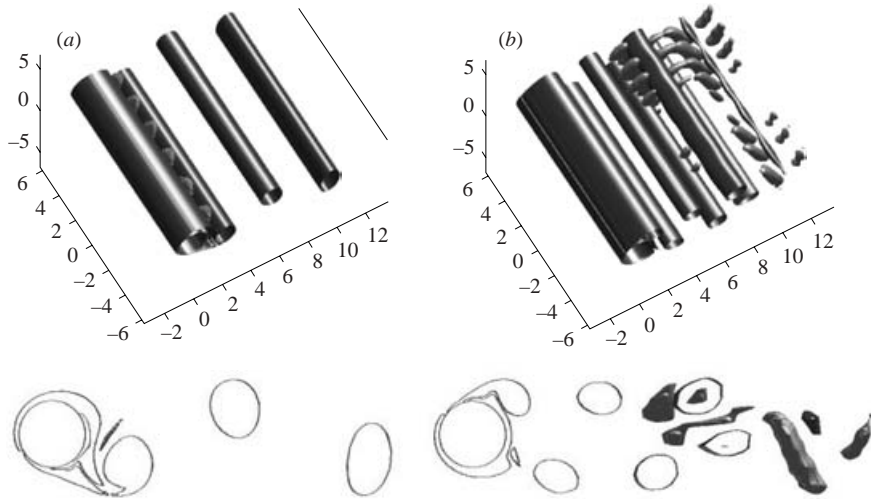


FIGURE 19. Localization of residual transverse vorticity, at  $t = 280$ . (a)  $S_F = S_t$  and  $A = \pi/2$ ,  $\omega^\perp = 0.25$ ; (b)  $S_F = 2S_t$  and  $A = \pi/7$ ,  $\omega^\perp = 0.1$ .

with respect to the amplitude  $A$ . This curve, plotted on figure 18, gives the mean remaining amount of non-axial vorticity, and its behaviour when the rotation amplitude  $A$  varies. This figure shows that this critical value makes a clear transition between two-dimensional flows (to the right of the critical value) and three-dimensional flows (to the left of the critical value).

## 7. Mechanisms involved in the return to a two-dimensional flow

From the numerical investigations performed above (at  $Re = 400$ ), one can identify two kinds of residual transverse vorticity.

These two states of residual three-dimensionality are described as follows. When the frequency is low (here at the natural frequency  $S_F = S_t$ ), a small amount of three-dimensionality remains close to the body, where gradients of vorticity are the strongest. When the frequency is higher (here at  $S_F = 2S_t$ ), residual three-dimensional structures are carried downstream, and seem to lose significance, at least up to an hypothetical critical distance, which is in any case outside the present computational domain. Snapshots of these two cases are shown on figure 19, which exhibits a low level of transverse isovorticity. Note that these levels are low, thus these two flows are close to a two-dimensional state.

In this section, we focus on the case  $S_F = 2S_t$  (since the harmonic case remains slightly three-dimensional). The return to a two-dimensional flow has already been quantified above by means of the transverse enstrophy  $Z^\perp$  (see § 5 and figure 13).

Before quantifying the mechanism leading to a two-dimensional flow, we can describe it qualitatively. We can guess from figure 20 that transverse eddies (non-spanwise structures of vortices) are carried downstream by the spanwise von Kármán streets. The strength of the von Kármán streets becomes greater when the cylinder is rotating, because the vorticity created in the boundary layer is  $\omega_z = -2\pi RL V_{\text{slip}}$  and tends to increase strength near the body.

In order to quantify this phenomenon, i.e. the fact that spanwise von Kármán streets carry the transverse eddies downstream, one can define two quantities, still

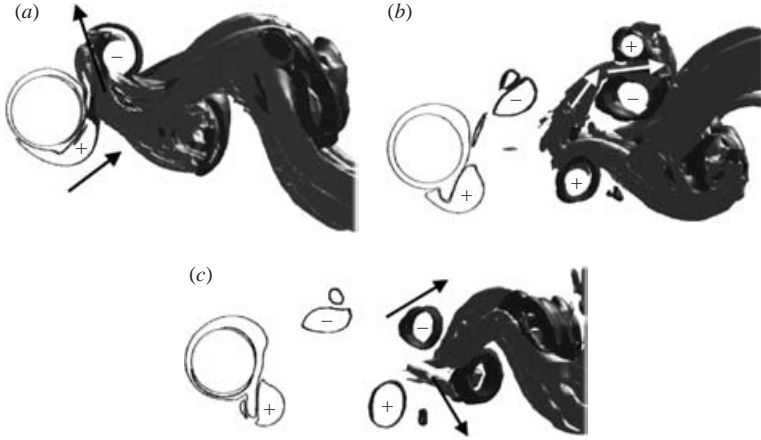


FIGURE 20. Motion of transverse eddies,  $Re = 400$ ,  $A = \pi/2$  and  $S_F = 2S_t$ . (a)  $t = 165$ , (b)  $t = 170$ , (c)  $t = 175$ .

based on partial values of the enstrophy. They are the *streamwise distribution of transverse vorticity*

$$F^\perp(r, t) = \int_0^L \int_0^{2\pi} \omega_x^2(r, \theta, z) + \omega_y^2(r, \theta, z) r \, d\theta \, dz \quad (7.1)$$

and the *streamwise distribution of spanwise vorticity*

$$F_z(r, t) = \int_0^L \int_0^{2\pi} \omega_z^2(r, \theta, z) r \, d\theta \, dz \quad (7.2)$$

which satisfy

$$\int_R^{R_\infty} F^\perp(r, t) + F_z(r, t) \, dr = 2Z.$$

The isovalues of these quantities give a good idea of the dynamics of transverse and spanwise eddies, providing a link between streamwise position and time. Moreover, a curve with a low value of  $F^\perp$  gives the evolution of the front of three-dimensionality, as plotted on figure 21. This figure shows both the curves  $F^\perp(r, t) = 0.25$  (evolution of the front of three-dimensionality) and  $F^\perp(r, t) = 20$  (evolution of the front of strong transverse eddies).

In order to study quantitatively the evolution of the front of transverse eddies, it is interesting to compare their dynamics with spanwise von Kármán street dynamics. This comparison is provided by means of the isovalue  $F_z(r, t) = 5$ , plotted on figure 22, which shows the evolution of the positions von Kármán streets. Both curves  $F_z(r, t) = 5$  and  $F^\perp(r, t) = 0.25$  are plotted on figure 22(b), on which it is rather clear that after  $t = 175$ , the front of transverse eddies is locked on von Kármán streets and is carried downstream.

Consequently, in this section, from now on, we aim to prove the following assertion: *the three-dimensional instabilities decrease in strength and are carried away in the stream when rotation frequency and amplitude are high enough. They finally disappear due to this transport phenomenon.* The fact that they decrease in strength and eventually

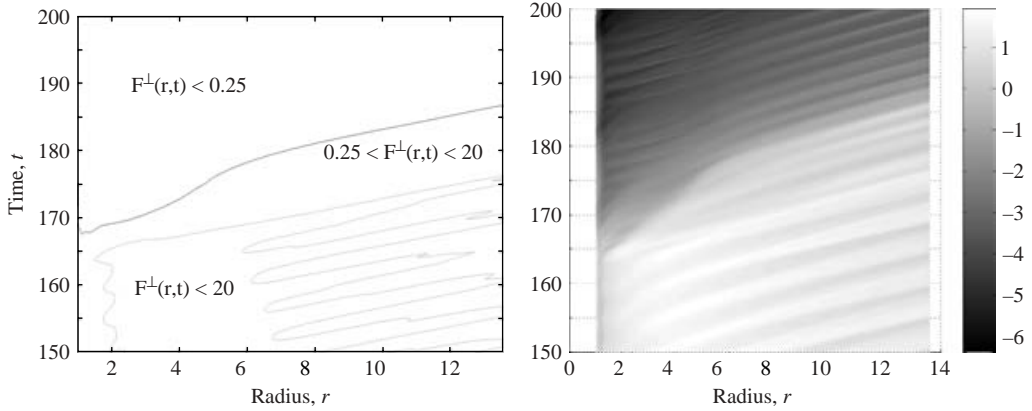


FIGURE 21. Dynamics of streamwise distribution of transverse vorticity  $F^\perp(r, t)$  at levels 0.25 and 20, for  $Re = 400$ ,  $A = \pi/2$  and  $S_F = 2S_t$ , rotation activated at  $t = 160$ . Colour bar:  $\text{Log}_{10} F^\perp(r, t)$ .

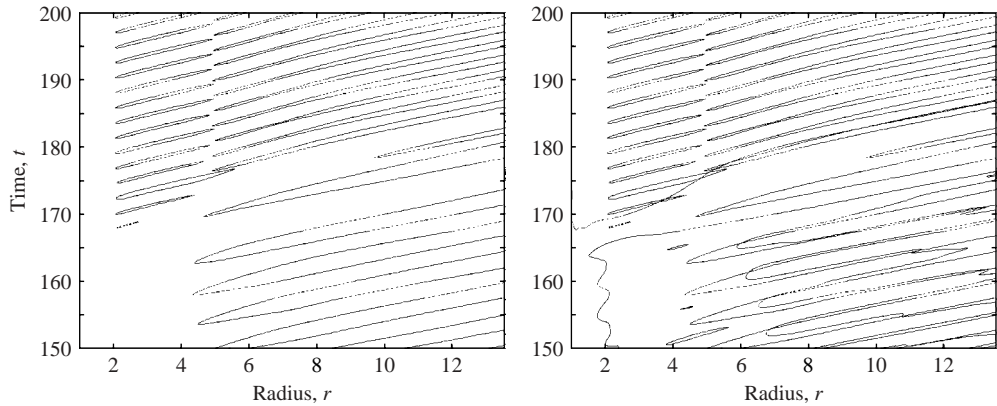


FIGURE 22. Dynamics of streamwise distribution of spanwise vorticity  $F_z(r, t)$ . The isovalue  $F_z(r, t) = 5$  is plotted in (a). In (b), the streamwise distribution of vorticity  $F^\perp(r, t)$  (from figure 21) is added. Same parameters as figure 21.

disappear is already proved because

$$F^\perp(r, t) \xrightarrow[t \rightarrow \infty]{} 0$$

for any  $r$ , as shown on figure 21.

In order to quantify the transport phenomenon, one removes the von Kármán street on which the front of instabilities seems to lock, and defines the *front location of spanwise eddies*

$$X_z(t) = \text{argmin}\{r \text{ such as } F_z(r, t) = 5\}$$

and the *front location of transverse eddies*

$$X^\perp(t) = \text{argmin}\{r \text{ such as } F^\perp(r, t) = 0.25\}$$

as shown on figure 23.

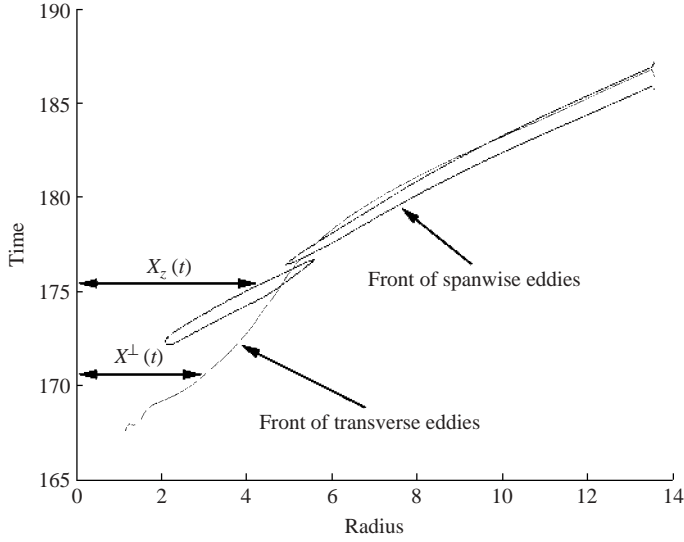


FIGURE 23. Definition of front location of spanwise ( $X_z(t)$ ) and transverse ( $X^\perp(t)$ ) eddies, respectively at level 5 and 0.25 (same parameters as figure 21).

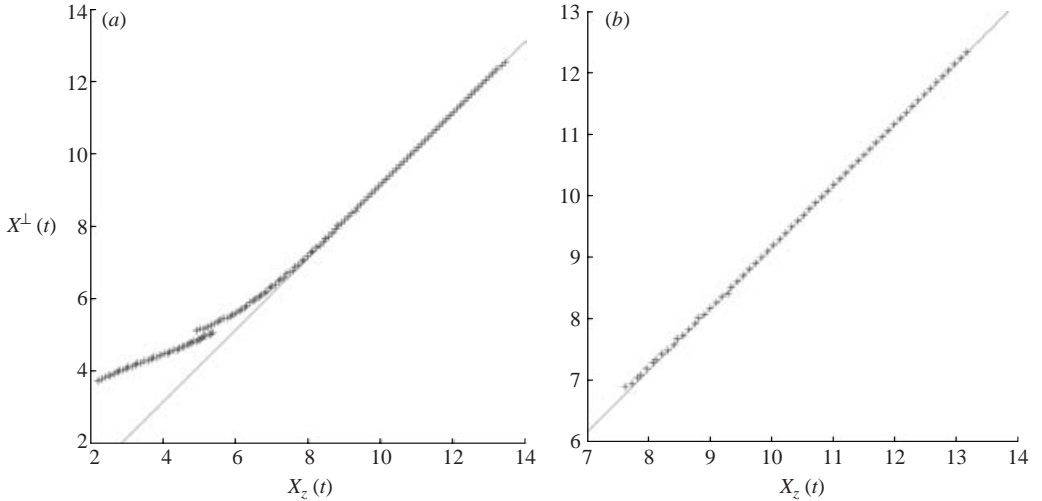


FIGURE 24. Front locations  $X^\perp(t)$  with respect to  $X_z(t)$  ((b) is a zoom of (a), parameters are the same as for figure 21).

These quantities are useful in the present case, because the assertion above that instabilities are captured by von Kármán streets is equivalent to a linear correlation between  $X_z$  and  $X^\perp$  over time. Figure 24 shows  $X^\perp$  with respect to  $X_z$ , and the dependence is clearly linear when  $r > 7R$ . One eventually obtains a correlation coefficient of 99.99%. The assertion is then proved to be valid, and the mechanism by which the instabilities disappear in the wake is identified. To conclude the present analysis, a comment on the domain of return to a two-dimensional flow is needed. An hypothetical critical distance from the body where the flow stays three-dimensional has been mentioned above. The enstrophy distribution, as a function of the distance from the body, is exponentially decreasing, thus reaching a value for which transverse



vortex structures are stable. Such a stability analysis requires very large domains with a control of the cells aspect ratio, which is not currently technically possible.

## 8. Conclusions

A Lagrangian numerical method has been developed to solve the fully nonlinear three-dimensional Navier–Stokes equations. The stability due to the implicit resolution of transport terms allows the use of large time steps. This means that one can compute and study the asymptotic behaviour in time of three-dimensional flows. The numerical scheme has been validated on both two-dimensional and three-dimensional diagnostics of flows behind a steady cylinder, and on two-dimensional flows past a rotating cylinder. The results obtained are consistent with some of the existing literature, numerical as well as experimental.

It has been shown, at  $Re = 400$ , that in a large neighbourhood of the body, the flow comes back to its nominal two-dimensional state all over the domain when the amplitude and frequency are high enough (here  $A = \pi/2$  and  $S_F/S_t = 2$ ). In this case, a substantial drop in the drag coefficient is seen, though not as dramatic as for experiments by Tokumaru & Dimotakis (1991) performed at  $Re = 15\,000$ .

When the forced and natural Strouhal numbers coincide, a small amount of three-dimensionality remains very close to the body (figures 11 and 19). The present results also validate two-dimensional numerical simulations of previous works, depending on the amplitude values.

A parametric study of the topology of the flow has then been performed at the first superharmonic frequency  $S_F/S_t = 2$ . A bifurcation diagram (figure 18) shows a clear transition between the resulting two-dimensional and three-dimensional flows. The different kinds of residual three-dimensionality have been shown and the mechanism leading to a two-dimensional state has been identified. This behaviour has not previously been shown numerically and seems to be a new contribution to the physics of the problem.

In summary, it has been shown by means of a parametric study that the wake generated by a translating and rotationally oscillating circular cylinder can lead either to a two-dimensional or a three-dimensional flow for the same Reynolds number, depending on the rotation parameters.

The author would like to acknowledge the invaluable help of Georges-Henri Cottet (University J. Fourier, Grenoble, France) and Petros Koumoutsakos (Institute of Computational Science, ETH Zürich, Switzerland), for their contributions in the preparation of this paper. The author would also like to thank Michele Milano (California Institute of Technology) for his helpful suggestions in the early development of this work. The computational resources have been provided by the joint CEA-UJF CIMENT-MIRAGE project, by the CEA-CENG (cluster IXIA), by the Department of Mathematics and Modelisation (INSA Toulouse, France) and CALMIP (CICT, Toulouse, France).

## REFERENCES

- BADR, H. M., COUTANCEAU, M., DENNIS, S. C. R. & MÉNARD, C. 1990 Unsteady flow past a rotating circular cylinder at Reynolds numbers  $10^3$  and  $10^4$ . *J. Fluid Mech.* **158**, 447–488.
- BADR, H. M. & DENNIS, S. C. R. 1985 Time-dependent viscous flow past an impulsively started rotating and translating circular cylinder. *J. Fluid Mech.* **158**, 447–488.

- BAEK, S. J. & SUNG, H. J. 1998 Numerical simulations of the flow behind a rotary oscillating circular cylinder. *Phys. Fluids* **10**, 869–876.
- BARKLEY, D. & HENDERSON, R. D. 1996 Three-dimensional Floquet stability analysis of the wake of a circular cylinder. *J. Fluid Mech.* **322**, 215–241.
- BEARMAN, P. 1997 Bluff body hydrodynamics. *Twenty-first Symposium on Naval Hydrodynamics, Trondheim, Norway*. National Academy Press.
- BEAUDAN, P. & MOIN, P. 1994 Numerical experiments on the flow past a circular cylinders at sub-critical Reynolds numbers. *Tech. Rep.* TF-62. Stanford University.
- BLACKBURN, H. M. & HENDERSON, R. D. 1999 A study of two-dimensional flow past an oscillating cylinder. *J. Fluid Mech.* **385**, 255–286.
- CHANG, C. C. & CHERN, R. L. 1991 Vortex shedding from an impulsively started rotating translating circular cylinder. *J. Fluid Mech.* **233**, 265–298.
- CHEN, Y. M., OU, Y. R. & PEARLSTEIN, A. J. 1993 Development of the wake behind a circular cylinder impulsively started into rotatory and rectilinear motion. *J. Fluid Mech.* **253**, 449–484.
- CHOU, M. H. 1997 Synchronization of vortex shedding from a cylinder under rotary oscillation. *Comput. Fluids* **26**, 755–774.
- COTTET, G.-H. & KOUMOUTSAKOS, P. D. 2000 *Vortex Methods, Theory and Practice*. Cambridge University Press.
- COTTET, G.-H., MICHAUX, B., OSSIA, S. & VANDERLINDEN, G. 2002 A comparison of spectral and vortex methods in three-dimensional incompressible flows. *J. Comput. Phys.* **175**, 702.
- COTTET, G.-H. & PONCET, P. 2002 Particle methods for Direct Numerical Simulations of three-dimensional wakes. *J. Turbulence* **3**(038), 1–9.
- COTTET, G.-H. & PONCET, P. 2003 Advances in Direct Numerical Simulations of three-dimensional wall-bounded flows by Particle in Cell methods. *J. Comput. Phys.* **193**, 136–158.
- COTTET, G.-H. & PONCET, P. 2004 New results in the simulation and control of three-dimensional cylinder wakes. *Comput. Fluids* **33**, 687–713.
- COUTANCEAU, M. & MÉNARD, C. 1985 Influence of rotation on the near-wake behind an impulsively started circular cylinder. *J. Fluid Mech.* **253**, 449–484.
- DEGOND, P. & MAS-GALLIC, S. 1989 The weighted particle method for convection-diffusion equations. *Math. Comput.* **53**, 485–526.
- DENNIS, S. C. R., NGUYEN, P. & KOCABIYIK, S. 2000 The flow induced by a rotationally oscillating and translating circular cylinder. *J. Fluid Mech.* **385**, 255–286.
- DÜTCH, H., DURST, F., BECKER, S. & LIENHART, H. 1998 Low-Reynolds-number flow around an oscillating circular cylinder at low Keulegan-Carpenter numbers. *J. Fluid Mech.* **360**, 249–271.
- FRIEDMANN, A. 1964 *Partial Differential Equations of Parabolic Type*. Prentice-Hall.
- GOVARDHAN, R. & WILLIAMSON, C. H. K. 2000 Modes of vortex formation and frequency response of a freely vibrating cylinder. *J. Fluid Mech.* **420**, 85–130.
- HE, J.-W., GLOWINSKI, R., METCALFE, R., NORDLANDER, A. & PERIAUX, J. 2000 Active Control and drag optimization for flow past a circular cylinder, I. Oscillatory cylinder rotation *J. Comput. Phys.* **163**, 83–117.
- HENDERSON, R. D. 1995a Adaptive spectral element methods for turbulence and transition. *Tech. Rep.* California Institute of Technology.
- HENDERSON, R. D. 1995b Details of the drag curve near the onset of vortex shedding. *Phys. Fluids* **7**, 2102–2104.
- HENDERSON, R. D. 1997 Nonlinear dynamics and patterns in turbulent wake transition. *J. Fluid Mech.* **352**, 65–112.
- HUERRE, P. & MONKEWITZ, P. A. 1990 Local and global instabilities in spatially developing flows. *Annu. Rev. Fluid Mech.* **22**, 473–537.
- JORDAN, S. 1997 Large-eddy simulation of the vortical motion resulting from flow over bluff bodies. *Twenty-first Symposium on Naval Hydrodynamics, Trondheim, Norway*. National Academy Press.
- JORDAN, S. K. & FROMM, J. E. 1972 Oscillatory drag, lift and torque on a circular cylinder in a uniform flow. *Phys. Fluids* **15**, 371–376.
- KANG, S., CHOI, H. & LEE, S. 1999 Laminar flow past a rotating cylinder *Phys. Fluids*. **11**, 3312–3321.
- KARNIADAKIS, G. & TRIANTAFYLLOU, G. 1992 Three-dimensional dynamics and transition to turbulence in the wake of bluff objects. *J. Fluid Mech.* **238**, 1–30.

- KOUMOUTSAKOS, P. D. & LEONARD, A. 1995 High-resolution simulations of the flow around an impulsively started cylinder using vortex methods. *J. Fluid Mech.* **296**, 1–38.
- KOUMOUTSAKOS, P. D., LEONARD, A. & PEPIN, F. 1994 Boundary conditions for viscous vortex methods. *J. Comput. Phys.* **113**, 52.
- KRAVCHENKO, A. G., MOIN, P. & SHARIFF, K. 1999 B-Spline method and zonal grids for simulations of complex turbulent flows. *J. Comput. Phys.* **151**, 757–789.
- LINDSAY, K. & KRASNY, R. 2001 A particle method and adaptive treecode for vortex sheet motion in three-dimensional flow. *J. Comput. Phys.* **172**, 879–907.
- LU, X. Y. & SATO, J. 1996 A numerical study of flow past a rotationally oscillating circular cylinder. *J. Fluids Struct.* **10**, 829–849.
- MILANO, M., GIANNAKOPOULOS, X., KOUMOUTSAKOS, P. & SCHMIDHUBER, J. 2000 Evolving strategies for active flow control. *Congress of Evolutionary Computations (CEC)*. IEEE Press, San Diego.
- MILANO, M. & KOUMOUTSAKOS, P. D. 2002 A clustering genetic algorithm for cylinder drag optimization. *J. Comput. Phys.* **175**, 79–107.
- MITTAL, R. 1996 Progress on LES of flow past a circular cylinder. *Annual Research Briefs*. Center for Turbulence Research.
- MITTAL, R. & BALACHANDAR, S. 1995 Effects of three-dimensionality on the lift and drag of nominally two-dimensional flows. *Phys. Fluid.* **7**, 1841–1865.
- MONAGHAN, J. J. 1985 Extrapolating B-Splines for interpolation. *J. Comput. Phys.* **60**, 253–262.
- OULD-SAHILI, M. L., COTTET, G.-H. & EL HAMRAOUI, M. 2000 Blending finite-differences and vortex methods for incompressible flow computations. *SIAM J. Sci. Comput.* **22**, 1655–1674.
- PERSILLON, H. & BRAZA, M. 1998 Physical analysis of the transition to turbulence in the wake of a circular cylinder by three-dimensional Navier-Stokes simulation. *J. Fluid Mech.* **365**, 23–88.
- PLOUMHANS, P. & WINCKELMANS, G. S. 2000 Vortex methods for high-resolution simulations of viscous flow past bluff bodies of general geometry. *J. Comput. Phys.* **165**, 354–406.
- PONCET, P. 2002 Vanishing of mode B in the wake behind a rotating circular cylinder. *Phys. Fluids* **14**, 2021–2024.
- PONCET, P. & COTTET, G.-H. 2003 Open-loop control of three-dimensional wakes. *Second MIT Conference, Boston, USA* (ed. K. J. Bathe), pp. 2348–2351. Elsevier.
- PONCET, P. & KOUMOUTSAKOS, P. 2004 Optimization of vortex shedding in three-dimensional wakes using belt actuators. *14th Intl Society of Offshore and Polar Engineering Conf. ISOPE 2004, Toulon, France* (ed. J. S. Chung, K. Izumiyama, M. Sayed & S. W. Hong), vol. 3, pp. 563–570. ISOPE.
- STRICKLAND, J. H., GRITZO, L. A., BATY, R. S., HOMICZ, G. F. & BURNS, S. 1999 Fast multipole solvers for three-dimensional radiation and fluid flow problems. In *Third Intl Workshop on Vortex Flows and Related Numerical Methods* (ed. A. Giovannini, G.-H. Cottet, Y. Gagnon, A. F. Ghoniem & E. Meiburg) *ESAIM Proc. Vol. 7*.
- SÜMER, B. M. & FREDSSØE, J. 1997 *Hydrodynamics around Cylindrical Structures*. World Scientific.
- TANEDA, S. 1978 Visual observations of the flow past a circular cylinder performing rotary oscillation. *J. Phys. Soc. Japan* **45**, 1038–1043.
- THOMPSON, M., HOURIGAN, K. & SHERIDAN, J. 1994 Three-dimensional instabilities in the wake of a circular cylinder. In *Proc. Intl Colloq. Jets, Wakes and Shear Layer, Victoria, Australia* (ed. K. Hourigan). CSIRO, Melbourne.
- THOMPSON, M., HOURIGAN, K. & SHERIDAN, J. 1996 Three-dimensional instabilities in the wake of a circular cylinder. *Expl. Therm. Fluid Sci.* **12**, 190–196.
- TOKUMARU, P. & DIMOTAKIS, P. 1991 Rotary oscillation control of a cylinder wake. *J. Fluid Mech.* **224**, 77–90.
- TOMBOULIDES, A., TRIANTAFYLLOU, G. & KARNIADAKIS, G. 1992 A new mechanism of period doubling in free shear flows. *Phys. Fluids A* **4**, 1329–1332.
- UNAL, M. F. & ROCKWELL, D. 1988 On vortex formation from a cylinder. Part I, the initial stability. *J. Fluid Mech.* **190**, 491–512.
- UTNES, T. 1997 Two-grid finite element formulations of the incompressible Navier–Stokes equations. *Commun. Numer. Meth. Engng* **13**, 675–684.
- WIESELSBERGER, C. 1922 New data on the laws of fluid resistance. *NACA Tech. Rep.* TN-84.
- WILLIAMSON, C. H. K. 1988 The existence of two stages in the transition to three-dimensionality of a circular cylinder. *Phys. Fluids* **31**, 3165–3168.
- WILLIAMSON, C. H. K. 1996 Three-dimensional wake behind a cylinder. *J. Fluid Mech.* **328**.